



**HOUSTON Gas Processors Association**  
YOUR MIDSTREAM NETWORK



**MUSE**  
**STANCIL**

# **GTL TECHNOLOGY UPDATE**

*Presented by:*

**Ajey Chandra**

**Managing Director  
Muse, Stancil & Co.**

**February 11, 2015**



# MUSE, STANCIL & Co.

---

➤ Independent energy consulting firm founded in 1984, providing industry expertise from wellhead to end-user; [www.musestancil.com](http://www.musestancil.com)

➤ **Energy Sectors Served**

- Natural Gas Processing
- Refining and Refined Products
- Pipelines
- Crude Oil
- Natural Gas Liquids
- Petrochemicals
- Biofuels

➤ **Representative Assignments**

- Market Studies
- Asset Valuation
- Project Development
- Transactional Due Diligence
- New Technology Assessment
- Insurance Claims (Property & Business Interruption)
- Litigation Support
- Royalty Negotiation/Auditing
- Contract Negotiation/Dispute Resolution



# GTL TECHNOLOGY UPDATE

---

- **Available gas “liquefaction” pathways**
  
- **Why GTL?**
  
- **Gas-To-Liquids Pathways**
  
- **Fischer Tropsch**
  - R&D work ongoing worldwide to increase efficiency in reaction pathway
  - Engineering design leading to more cost effective process design
  
- **New market entrants**

# GAS LIQUEFACTION PATHWAYS

- **Variety of technology pathways exist for conversion of commercial natural gas to various liquid products**
  - Natural Gas Liquefaction (LNG)
  - Natural Gas Conversion
    - Natural Gas to Methanol (GTM)
    - GTM integrated with Methanol to Gasoline (MTG) or other products such as dimethylether (DME)
  
- **Comparison of Netback Prices, Basis: 2014 Averages and Henry Hub**

	<i>LNG to Europe</i>	<i>LNG to Asia</i>	<i>Methanol</i>	<i>GTL</i>
Product Sales Price	\$9.69/MMBTU	\$15.78/MMBTU	\$443.35/MT	\$104.09/BBL
U.S. Dollars Per MMBTU gas processed				
Revenue	8.73	14.21	13.64	10.41
Shipping	(1.00)	(2.80)		
Tolling	(2.75)	(2.75)	(9.11)	(5.49)
Netback per MMBTU	4.98	8.66	4.53	4.92

# GAS LIQUEFACTION PATHWAYS

- **Variety of technology pathways exist for conversion of commercial natural gas to various liquid products**
  - Natural Gas Liquefaction (LNG)
  - Natural Gas Conversion
    - Natural Gas to Methanol (GTM)
    - GTM integrated with Methanol to Gasoline (MTG) or other products such as dimethylether (DME)
  
- **Comparison of Netback Prices, Basis: 2014 Averages and Henry Hub**

	<i>LNG to Europe</i>	<i>LNG to Asia</i>	<i>Methanol</i>	<i>GTL</i>
Product Sales Price	\$9.69/MMBTU	\$15.78/MMBTU	\$443.35/MT	\$104.09/BBL
U.S. Dollars Per MMBTU gas processed				
Revenue	8.73	14.21	13.64	10.41
Shipping	(1.00)	(2.80)		
Tolling	(2.75)	(2.75)	(9.11)	(5.49)
Netback per MMBTU	4.98	8.66	4.53	4.92

***Production of GTL diesel is competitive with other liquefaction pathways; specific project economics can vary significantly***

# WHY GTL?

---

## ➤ **“Stranded” Gas**

- Geographically isolated gas deposits
- Gas reserves with limited economic market accessibility
- Gas flaring

## ➤ **Diesel Markets**

- Strong diesel demand world wide
- Emphasis on increasingly “cleaner” diesel fuel worldwide
- Significant change in the gasoline/diesel price relationship since 2008

# WHY GTL?

---

## ➤ “Stranded” Gas

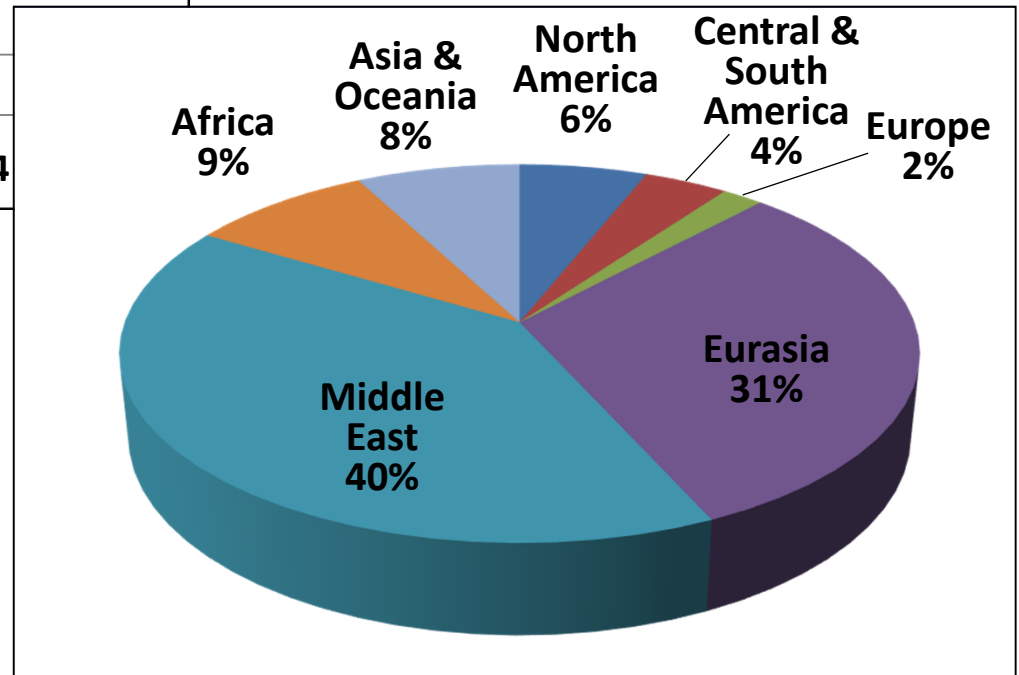
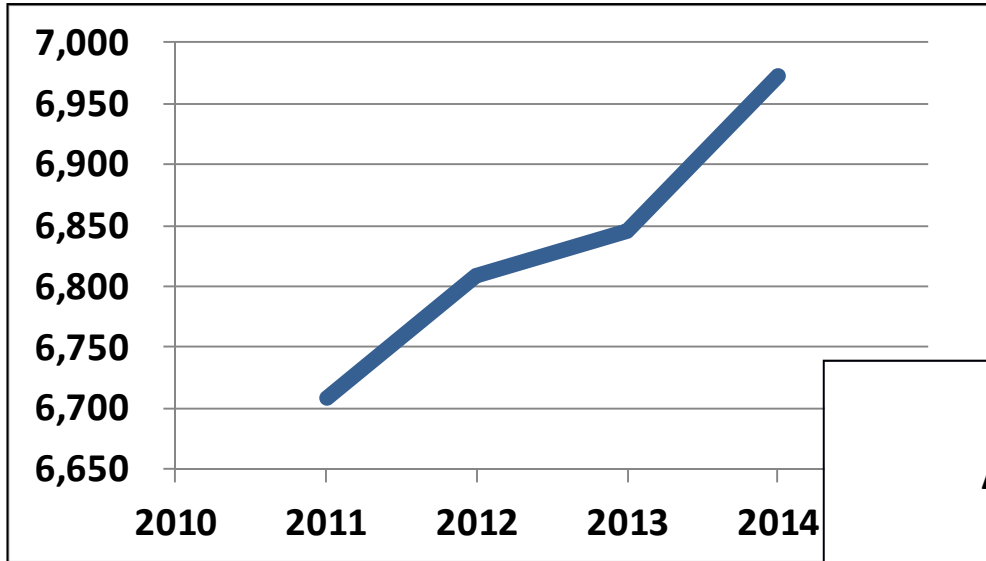
- Geographically isolated gas deposits
- Gas reserves with limited economic market accessibility
- Gas flaring

## ➤ Diesel Markets

- Strong diesel demand world wide
- Emphasis on increasingly “cleaner” diesel fuel worldwide
- Significant change in the gasoline/diesel price relationship since 2008

***Small-scale, compact and mini-GTL enable project development in a wide variety of locations both onshore and offshore***

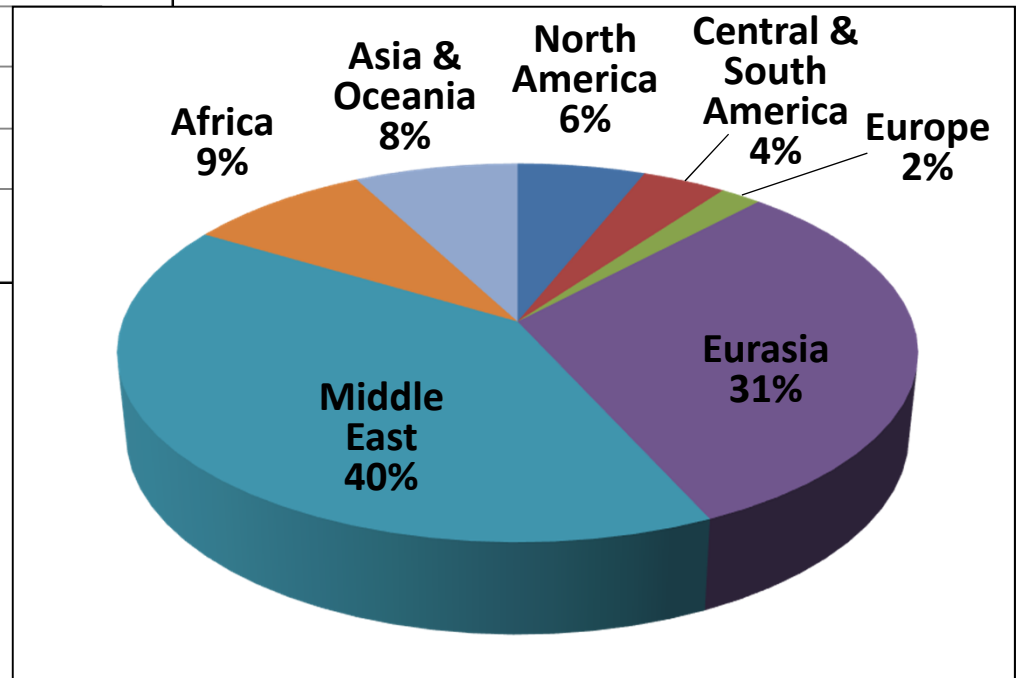
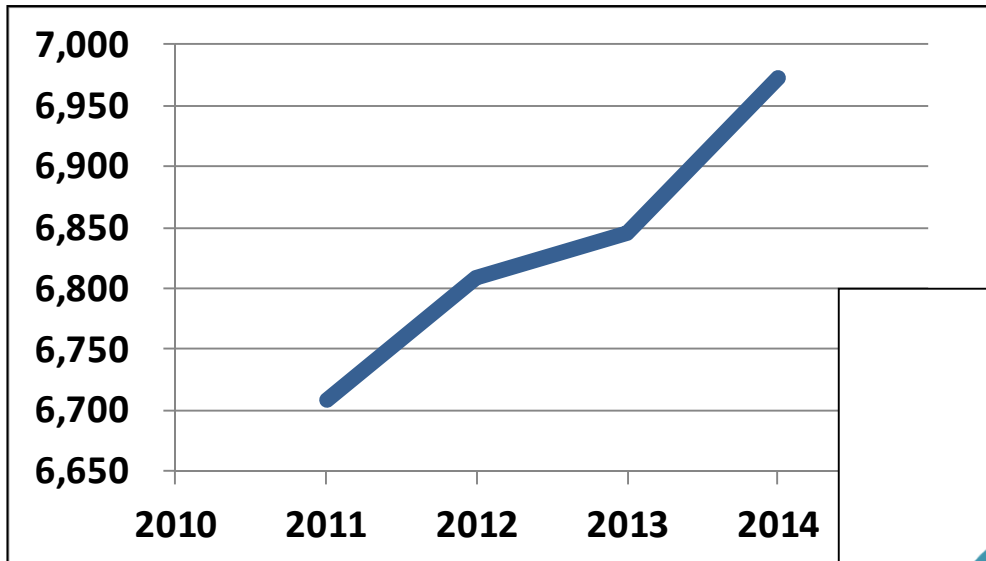
# WORLDWIDE GAS RESERVES



- Large-scale GTL already in service in Qatar
- LNG projects dominate Asia & Oceania



# WORLDWIDE GAS RESERVES



- Large-scale GTL already in service in Qatar
- LNG projects dominate Asia & Oceania

***BUT...many opportunities exist to deploy smaller-scale GTL worldwide***

# GTL PRODUCTS EXCEED STRINGENT QUALITY REQUIREMENTS

---

	<i>GTL</i>		<i>CARB</i>	
	<i>Diesel</i>	<i>ULSD</i>	<i>Diesel</i>	<i>Jet</i>
Sulfur, ppm max	<1	10	8	3000
Aromatics, max	0%	31.7%	10%	25%
Gravity, API		30+	30+	37-51
Cetane Number, min	74+	40	40	40

Note: ULSD and Jet specifications based on Colonial Pipeline 12/2011 specifications  
CARB Diesel specification based on Kinder Morgan Pipeline specification

# GTL PRODUCTS EXCEED STRINGENT QUALITY REQUIREMENTS

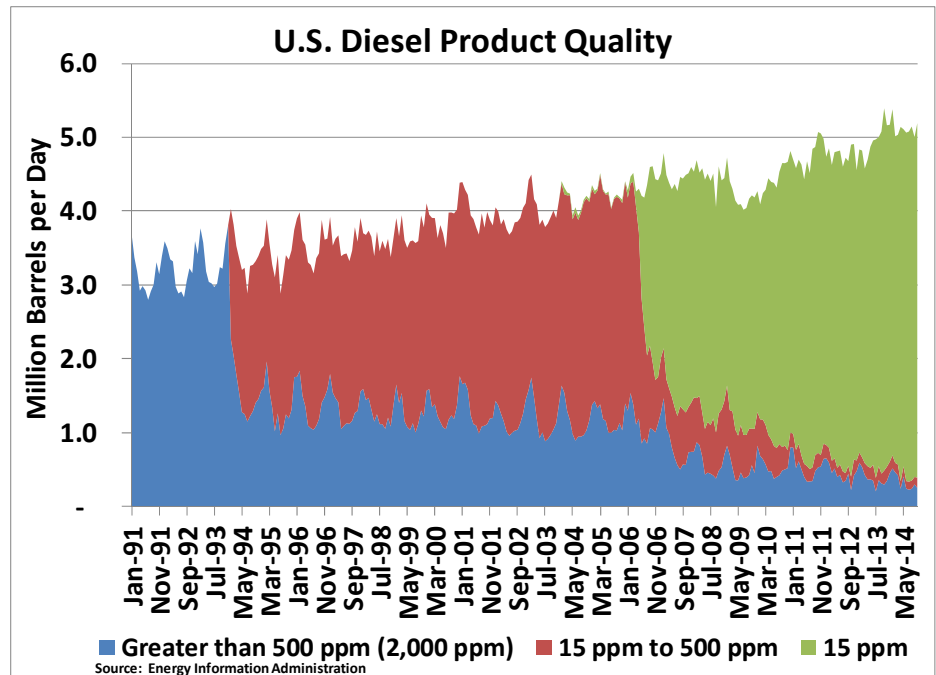
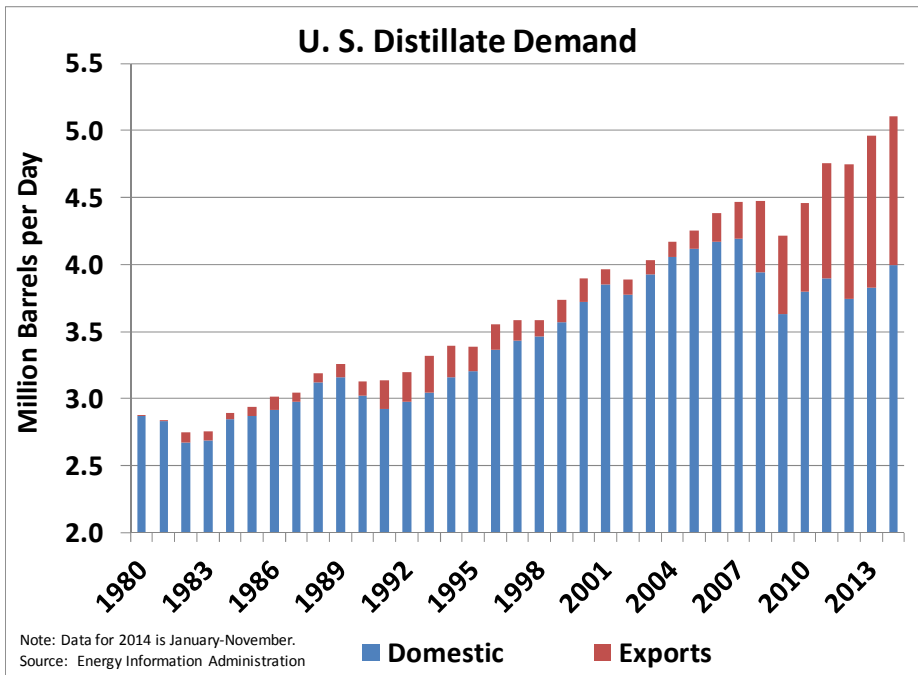
	<i>GTL</i>		<i>CARB</i>	
	<i>Diesel</i>	<i>ULSD</i>	<i>Diesel</i>	<i>Jet</i>
Sulfur, ppm max	<1	10	8	3000
Aromatics, max	0%	31.7%	10%	25%
Gravity, API		30+	30+	37-51
Cetane Number, min	74+	40	40	40

Note: ULSD and Jet specifications based on Colonial Pipeline 12/2011 specifications  
CARB Diesel specification based on Kinder Morgan Pipeline specification

***GTL produces a perfectly fungible fuel  
and, therefore, GTL products can be supplied  
into almost any market***

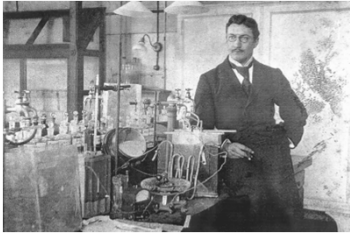
# DEMAND GROWTH FOR HIGHEST QUALITY PRODUCT

- Air quality concerns have driven global diesel requirements toward very low sulfur, low aromatic product specifications
- The U.S. demand for diesel is growing and U.S. refiners are also exporting huge volumes of higher quality diesel fuels
- These trends are expected to continue

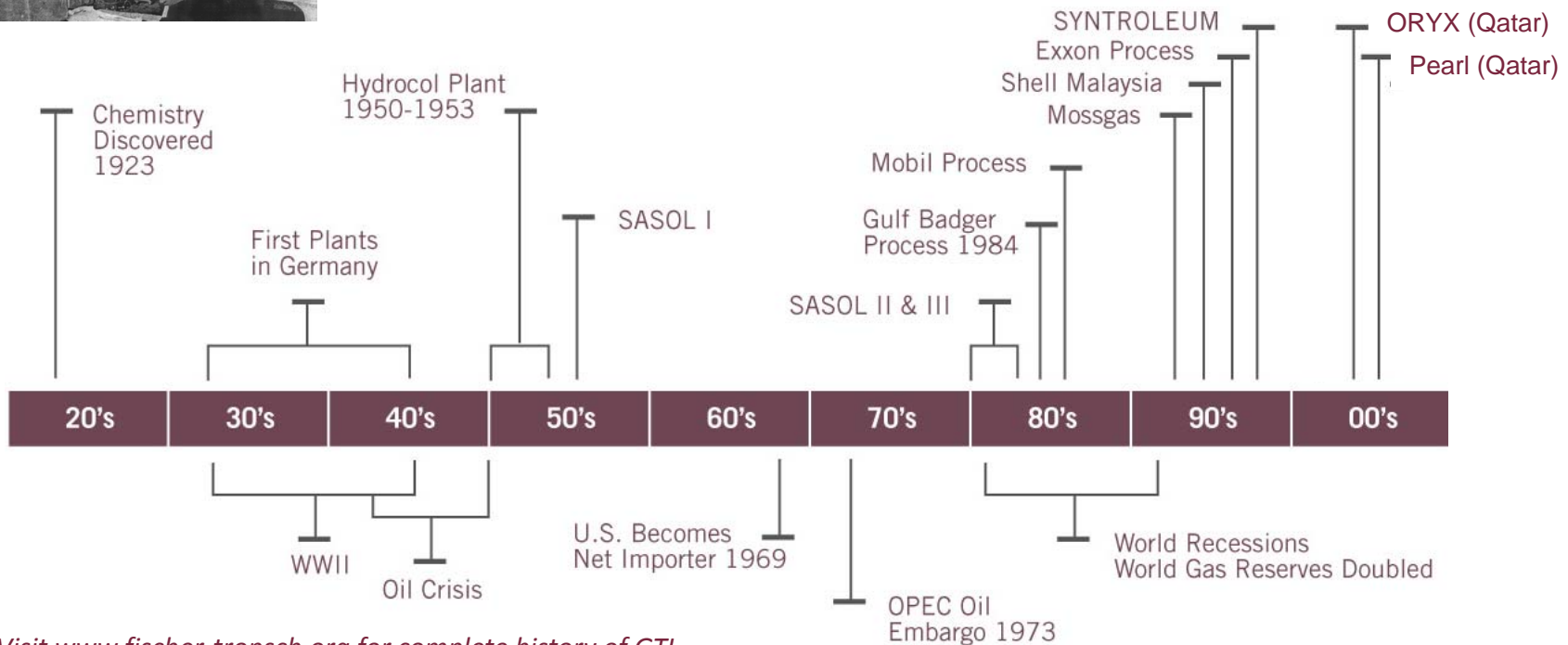


# NATURAL GAS TO DIESEL (GTL) – WELL ESTABLISHED AND PROVEN

## History



**Franz Fischer**  
1918 – “Father” of GTL



Visit [www.fischer-tropsch.org](http://www.fischer-tropsch.org) for complete history of GTL

**Advances in catalyst development and process design are fueling expansion in small-scale GTL sector**

# NUMEROUS COMPANIES DEVELOPING MINI-GTL TECHNOLOGY

---



GRT, Inc.

VERDIS  
SYNTHETIC FUELS



# NEW ENTRANTS IN THE MARKET FOR MINI-GTL

Company	Technology	Notes
INFRA	FT	100 BPD plant (2015)
Greyrock	FT	1000 BPD plant (2015)
Emerging Fuel Tech. (EFT)	FT	1 BPD pilot plant
Gas2	FT	3 BPD pilot
Marcellus GTL	MTG	2000 BPD (2016)
TIGAS	MTG	Demo plant in Houston
Primus GE	MTG	6.5 BPD plant in operation
TU Freiberg	MTG	15 BPD plant
Siluria	OCM	1 TPD ethylene pilot plant being constructed
Proton Ventures	Small scale Ammonia	0.2 MMcfd feed rate (3 TPD Ammonia)

# POSITIVE ATTRIBUTES

---

- **Proven chemistry**
- **Years of bench-scale testing, industry has “fine tuned” catalyst and commercialized catalyst manufacturing**
- **Scale-up of most of the process components already proven**
  - Production of syngas, front end
  - Hydrocracking of wax and distillation of products, back end
- **GTL-FT diesel product has been tested in many commercial applications**
  - Commercial Aircraft
  - Trucking Industry
  - Military, B52 Bomber
- **Commercial plants have operated in South Africa for many years**



# CHALLENGES

---

- **Capital cost for fixed-bed reactor processing configuration historically dictated larger projects to capture economies of scale; largest world-scale project completed to date far exceeded budget estimate**
- **Margin risk associated with uncorrelated feedstock and product price volatility**
- **Catalyst selectivity for wax production versus direct conversion to diesel or gasoline**
- **Scale-up of high efficiency, fluidized bed reactors not proven thus complicating process technology guarantees and project finance**
  - Physical design, wax separation from catalyst particles
  - Heat balance, highly exothermic reaction requires active control of heat balance to avoid “hot spots”

# CHALLENGE – CAPITAL COST

---

- **Number of companies developing modular process design**
- **Minimize “custom” aspects of project design**
- **Provide for shop fabrication to improve quality control and compress projection execution timeline**
- **With modular approach, smaller projects become economically feasible**
- **In addition, developer are seeking brownfield sites or have partnered with integrated producers to integrate smaller-scale commercial units into existing facilities**

# CHALLENGE – MARGIN RISK

---

- **AGE OLD QUESTIONS – What will oil and gas prices be next week? Next month? Next year? In 5 years? In 10 years?**
  
- **Commercial viability of small-scale units requires venture capital support; technical advances in reactor design are enabling such projects**
  
- **Project finance will require positive economic margin outlook in the medium to long term**
  
- **Opportunities enabled by new reactor design technologies include:**
  - Offshore or floating installations
  - Focus on “portable” nature of the process
  - Remote locations where liquid takeaway infrastructure is available or can be installed at lower cost than can gas infrastructure
  - In many locations worldwide where gas flaring is being severely limited

# CHALLENGE – CATALYST DEVELOPMENT

---

- **All GTL catalysts are proprietary although most GTL companies have one or two catalyst manufactures who are licensed to produce**
  
- **Most recent leap forward is catalyst for direct conversion of natural gas to diesel, thus eliminating the wax step**
  - Will likely result in reduced capital cost for less complex “back end” of the process
  - May also have implications for reactor design and ultimate reactor scale up, yet to be determined
  
- **INFRA**
  - Announced investment decision on 100 BPD plant in June
  - Pilot Plant launch in July
  - Will test additional catalysts and plant configurations
  
- **Greyrock**
  - Direct-to-Diesel™ Catalyst
  - Modular construction of a 1,000 BPD plant
  - Capacity can be increased by adding additional modules
  - “Drop in” fuel which has been tested in heavy duty engines

# NON-FT PROCESSES - GAS TO CHEMICALS AND GASOLINE

---

## ➤ **Primus Green Energy**

- 6.5 BPD pilot plant was commissioned in 2013
- Currently in third continuous run
- Producing 93 octane gasoline

## ➤ **TIGAS**

- Conversion to gasoline in a single synthesis loop with no need for methanol storage

## ➤ **Proton Ventures**

- Gas2Ammonia process

## ➤ **Siluria**

- Conversion of methane and ethane into gasoline and ethylene

# CHALLENGE – REACTOR SCALE-UP

---

- **Process developers have been mindful of the need for measured scale-up with respect to fluidized-bed reactors**
- **Some demonstration scale units have been built and operated to prove aspects of reactor engineering design**
- **To address the issue of clean wax separation from catalyst particles, new catalysts are being developed to eliminate the wax production and directly produce diesel; development work continues and the industry awaits commercially-available data on these new catalysts**
- **Other developers have focused on innovative changes in fixed bed reactor design developing modular, micro channel reactors**
- **Pilot plant and demonstration-scale plants employing micro-channel reactor technology have operated and larger scale commercial projects are being developed**
  - Velocycs
  - Compact GTL

# CONCLUSIONS

---

- **A wide variety of options exist for GTL projects**
- **Large increase in gas supply in North America has increased the attractiveness of these projects**
- **While LNG and large scale GTL projects continue, the newer technology is aimed at mini GTL plants that can be built with smaller gas reserves**
- **The smaller units provides good economics by being modular and skid mounted, so they can be constructed in areas that provide market opportunities**
- **New technologies are in various stages of commercialization, and there are several very promising start-ups competing for investment funds**